

Low Energy Desalination Options to Eliminate Sulfates from Discharge

Patrick Curran

Senior Partner

Archimedes Industrial Advisory & Investment

patrick@aiaigrp.com

001-949-302-5265



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Problem: Reduced sulfate discharge limits, permits

> 30% sulfates come from drained acid

About 1/3 of sulfates in discharge comes from neutralization of drained acid in flooded batteries. Less for AGM.

Neutralized acid is hypersaline

Typically the neutralized water or scrubber blowdown is > 60,000 ppm

Treat with caustic or ammonia

Whether treated with caustic or ammonia, a high salinity liquid is produced.



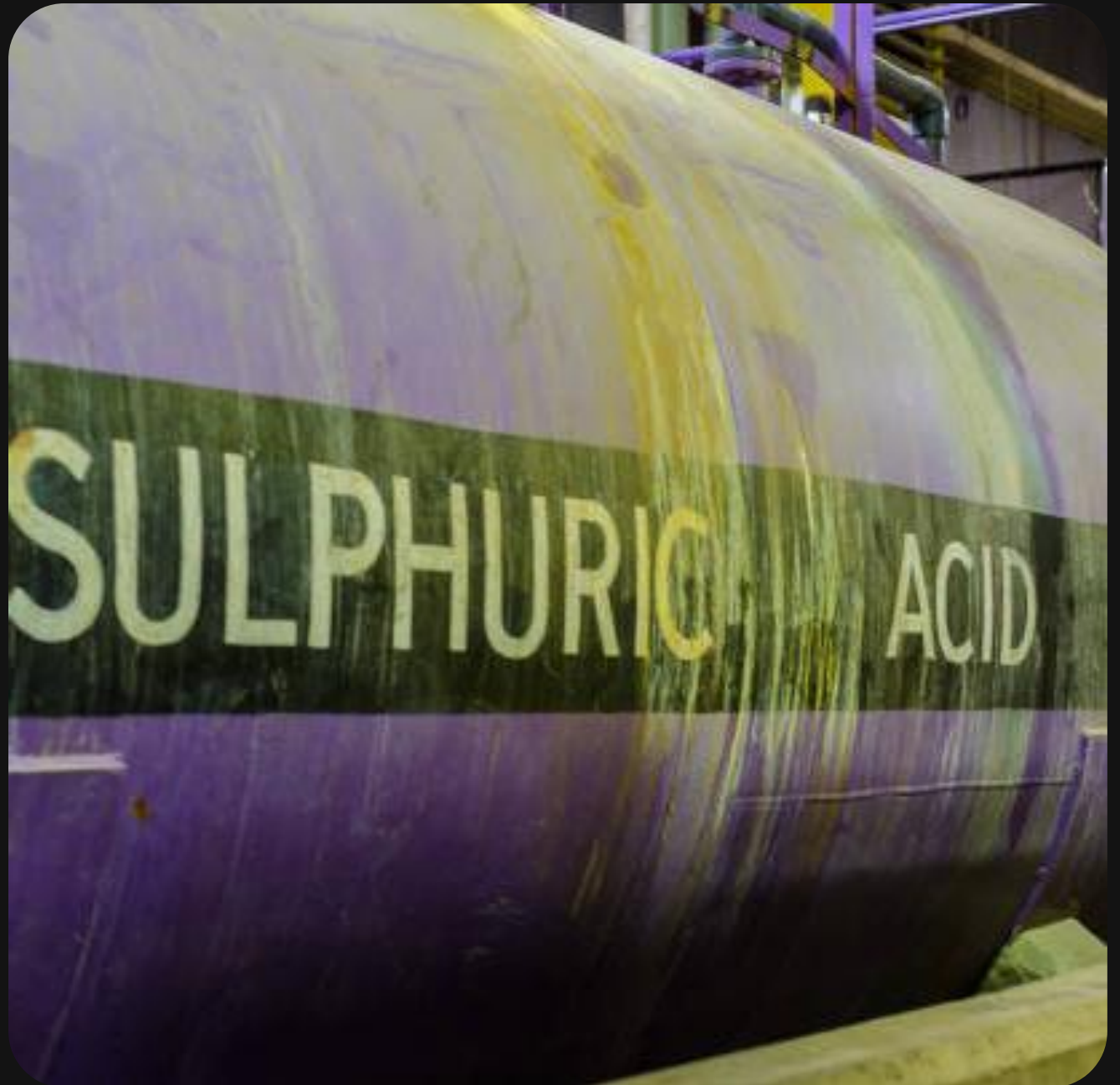
Stop neutralizing acid and solve > 30% of the problem!

It's not a technology problem

There are commercially available technologies that can clean and concentrate the acid.

It's a logistics problem

Need to find a home and match the process to the client specifications.



TECHNOLOGY READINESS LEVEL (TRL)

RESEARCH	9	ACTUAL SYSTEM PROVEN IN OPERATIONAL ENVIRONMENT
	8	SYSTEM COMPLETE AND QUALIFIED
	7	SYSTEM PROTOTYPE DEMONSTRATION IN OPERATIONAL ENVIRONMENT
DEVELOPMENT	6	TECHNOLOGY DEMONSTRATED IN RELEVANT ENVIRONMENT
	5	TECHNOLOGY VALIDATED IN RELEVANT ENVIRONMENT
	4	TECHNOLOGY VALIDATED IN LAB
DEPLOYMENT	3	EXPERIMENTAL PROOF OF CONCEPT
	2	TECHNOLOGY CONCEPT FORMULATED
	1	BASIC PRINCIPLES OBSERVED

Technology options to treat hypersaline discharge

- **Mechanical Vapor Recompression with Crystallizer. TRL-9**
- **Ultra High-Pressure Reverse Osmosis. TRL-8**
- **Electro Hydrodynamic Evaporation. TRL-7**
- **Cavitation. TRL - 6**



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Mechanical Vapor Recompression with Crystallizer

- **Most common technology set to treat hypersaline brine**
- **Produces clean water and dry salt (ZLD)**
- **MVR stage concentrates the brine, crystallizer drops out the salts**
- **High capital costs - \$375,000 per m³**
- **High energy usage – 80 kWhr/m³**
- **High maintenance due to exotic alloys and moving parts**
- **High cost of ownership.**



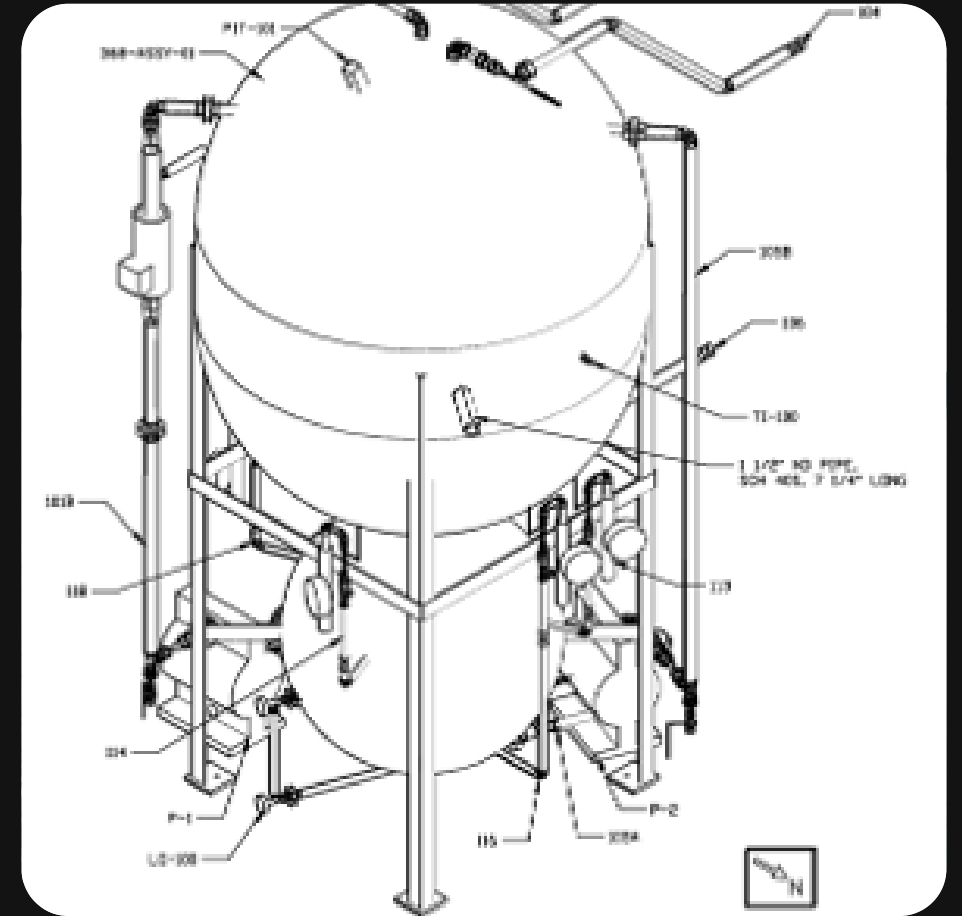
Ultra High-Pressure Reverse Osmosis

- Can treat up to 60,000 ppm inlet water
- Produces super brine and clean water
- MLD (minimal liquid discharge), requires additional processes to produce dry salts such as crystallizer
- Low capital costs - \$44,000 per m³ by itself
- Low energy usage – 5 kWhr/m³ by itself
- Medium maintenance for membranes



Electro Hydrodynamic Evaporation

- Produces clean vapor and dry salt (ZLD)
- Single stage process
- Medium capital costs - \$54,000 per m³
- Low energy usage – 20 kWhr/m³
- Low maintenance due low pressure and few moving parts
- Low cost of ownership



Hydrodynamic Cavitation

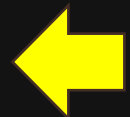
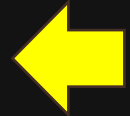
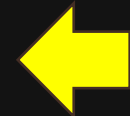
- Produces partially desalinated water plus dry salts
- Requires additional process such as UHPRO & MVR
- Low capital costs - \$35,000 per m3
- Low energy usage – 4 kWhr/m3
- Low maintenance due to simple pump and nozzle
- Low cost of ownership



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Normalized Cost of Ownership Comparison

Technology	Addition Process Needed	Energy (USD/m ³)	Deprec (USD/m ³)	Mainten (L/M/H)	Cost of Ownership (USD/m ³)	MVR-Cryst Comparison
MVR Crystallizer	None	\$12.00	\$2.16	\$6.49	\$20.66	---
Ultra High- Pressure RO	Crystallizer	\$6.75	\$1.59	\$4.77	\$12.74	-38.3%
Electro Hydrodynamic Evaporation	None	\$3.00	\$0.89	\$1.78	\$5.67	-72.5%
Cavitation	UHPRO & Crystallizer	\$3.56	\$1.00	\$3.00	\$7.56	-63.4%



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Conclusions

Isolate acid & treat

This will reduce sulfates to be treated by at least 30%

High TRL Alternatives

There are high TRL options that can lower cost of ownership by up to 72%.

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